

## Klea® 407C Physical Property Data Sheet – British Units

Klea® 407C is a blend of HFCs 32, 125 and 134a designed to replace HCFC-22 in new air conditioning and low temperature refrigeration equipment and also for retrofit in many existing systems. Klea® 407C offers the optimal combination of minimal environmental impact with favorable technical performance. For information on the properties and safe handling of Klea® 407C, please refer to the Material Safety Data Sheet supplied with the product or available upon request.

The data presented here represents a combination of measurements and estimation. Mexichem does not guarantee its accuracy and reserves the right to update the information in the future, in light of the best available knowledge at the time.

### Physical Property Data for Klea® 407C

Property		Units	Value
Bubble Point	(1atm)	°F	-47.2
Dew Point	(1atm)	°F	-34.2
Bubble Point Pressure	(70°F)	psia	156
Estimated Critical Temperature		°F	187
Latent Heat Vaporization	(Tm=70°F)	Btu/lb	85.3
Trouton's Constant		Btu/lb R	0.265
Coeff. Vol. Therm. Exp.	(liquid, 60°F)	°R <sup>-1</sup>	0.0019
Density		lb/ft <sup>3</sup>	0.285

### Equation of State (Martin-Hou)

$$Pr = \frac{XT_r}{V_r - B} + \sum_{i=1,4} \frac{(A_i + B_i Tr + C_i \exp(-KT_r))}{(V_r - B)^{(i+1)}}$$

$$T_r = T/T_c, P_r = P/P_c, V_r = V/V_c$$

$$X = 3.649216$$

$$B = 0.0$$

$$K = 5.475$$

$$T_c, P_c, V_c = 646.6, R 674.7 \text{ psia}, 0.0327 \text{ cu. Mb}$$

$$A_1, B_1, C_1 = -11.576411672, 6.9516394791, -12.992106787$$

$$A_2, B_2, C_2 = 9.108927853, -5.8551996466, -101.85219827$$

$$A_3, B_3, C_3 = -4.2674117378, 0.0, 0.0$$

$$A_4, B_4, C_4 = 17.976354749, 0.0, -1992.5643203$$

Applicable Range: 0-400 psia, 0-180 R superheat

### Saturation Envelope — Bubble Point Temperatures

$$\text{Bubble Point Temperature } (T_b) = A + BX + CX^2 + DX^3 + EX^4$$

$T_b$  = Bubble Point Temperature in °F

$X = \ln(P)$

$P$  = Pressure in psia

$A = -123.1417$

$B = 19.59164$

$C = 3.35685$

$D = -0.181209$

$E = 0.049304$

### Saturation Envelope — Dew Point Temperatures

$$\text{Bubble Point Temperature } (T_d) = A + BX + CX^2 + DX^3 + EX^4$$

$T_d$  = Dew Point Temperature in °F

$X = \ln(P)$

$P$  = Pressure in psia

$A = -119.0841$

$B = 31.31686$

$C = -1.91995$

$D = 0.804863$

$E = -0.020383$

### Saturation Envelope — Mid Point Temperatures

$$\text{Mid Point Temperature } (T_m) = A + BX + CX^2 + DX^3 + EX^4$$

$T_m$  = Mid Point Temperature in °F

$X = \ln(P)$

$P$  = Pressure in psia

$A = -121.1129$

$B = 25.45425$

$C = 0.718449$

$D = 0.311827$

$E = 0.0144605$

### Latent Heat Vaporization

$$dh_{\text{latent}} = A + BX + CX^2 + DX^3 + EX^4$$

$A = 94.0883061$

$B = -723.65623$

$C = 2719.42721$

$D = -3539.0967$

$E = 1670.0172$

$T_m$  = Mid Point Temperature R

$T_c$  = Critical Temperature R

$T_c^c$  = Critical Temperature R

$T_c = 646.6$  R

$dh_{\text{latent}} = \text{Btu/lb}$

### Ideal Gas Heat Capacity

$$C_p(\text{ideal}) = A + BT + CT^2 + D/T^3 + D/T$$

A = -2.002556E-2	T = Temperature R
B = 4.26626E-4	$C_p(\text{ideal}) = \text{Btu/lb R}$
C = -1.430584E-7	
D = 15.630503	

### Saturated Liquid Enthalpy

$$h_{\text{liquid}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{where } x = (1 - (T_b/T_c))^{(1/3)}$$

A = 37.5396507	$T_b = \text{Bubble Point Temperature R}$
B = 526.55632	$T_c = \text{Critical Temperature R}$
C = -1811.0258	$T_c = 646.6 \text{ R}$
D = 2169.01685	$h_{\text{liquid}} = \text{Btu/lb}$
E = -1087.0894	

### Liquid Density

$$P_{\text{liquid}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{where } x = (1 - (T_b/T_c))^{(1/3)}$$

A = -40.606805	$T_b = \text{Bubble Point Temperature R}$
B = 490.787461	$T_c = \text{Critical Temperature R}$
C = -955.92001	$T_c = 640.6 \text{ R}$
D = 980.476064	$P_{\text{liquid}} = \text{lb/ft}^3$
E = -357.97408	

### Liquid Viscosity

$$\ln(\mu)_{\text{liquid}} = A + B/T_m + CT_m + D/T_m$$

A = 15.66442	$\mu_{\text{liquid}} = \text{cP}$
B = -2309.4954	$T_m = \text{Mid Point Temperature R}$
C = -0.0341689	
D = 0.00001796	

### Liquid Thermal Conductivity

$$K_{(\text{liquid})} = A + BT_m + CT_m^2 + D/T_m^3$$

$$\text{where } x = (1 - (T_m/T_c))^{(1/3)}$$

A = 0.06874537	$T_m = \text{Mid Point Temperature R}$
B = 0	$K_{(\text{liquid})} = \text{Btu/hr.ft.R}$
C = -1.198298E-7	
D = 9.40172848	

**Saturated Vapor Density**

$$P_{\text{vapor}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{Where } x = (1 - (T_d/T_c))^{(1/3)}$$

A = 19.6903406	T <sub>d</sub> = Dew Point Temperature R
B = 21.4442365	T <sub>c</sub> = Critical Temperature R
C = -242.43767	T <sub>c</sub> = 646.6 R
D = 348.817574	P <sub>vapor</sub> = lb/ft <sup>3</sup>
E = -146.90014	

**Vapor Viscosity (Ideal Vapor)**

$$\mu_{\text{vapor}} = A + BT + CT^2$$

A = -0.0013724	T = Temperature R
B = 0.00002977	$\mu_{\text{vapor}} = \text{cP}$
C = -4.726E-09	

**Vapor Viscosity (Sat Vapor)**

$$\mu_{\text{vapor}} = A + BT_d + CT_d^2 + DT_d$$

A = 0.375554	$\mu_{\text{vapor}} = \text{cP}$
B = -0.0007599	TD = Dew Point Temperature R
C = 5.489E-07	
D = -60.07482	

**Vapor Thermal Conductivity (Ideal Vapor)**

$$K_{\text{vapor}} = A + BT + CT^2$$

A = -2.054908E-3	T = Temperature R
B = 1.1506995E-5	K(vapor) = Btu/hr.ft.R
C = 1.3817671E-8	

**Vapor Thermal Conductivity (Sat Vapor)**

$$K_{\text{vapor}} = A + BT_d + CT_d^2 + D/T_d$$

A = 0.24578002	K(vapor) = Btu/hr.ft.R
B = -5.0217916E-4	T <sub>d</sub> = Dew Point Temperature R
C = 3.7181456E-7	
D = -40.089109	

**Speed of Sound (Sat Vapor)**

$$\mu_{(\text{vapor})} = A + BT_d + CT_d^2 + D/T_d$$

A = -2854.0469  
 B = 8.98147237  
 C = -7.595246E-3  
 D = 406179.685

$\mu_{(\text{vapor})} = \text{ft/s}$   
 T<sub>d</sub> = Dew Point Temperature R

**Liquid Properties**

Temp °F	Liquid Density lb/ft <sup>3</sup>	Liquid Enthalpy Btu/lb	Latent Heat Btu/lb	Liquid Viscosity cP	Liq Therm Cond Btu/hr.ft.R
-60	87.55	-6.58	111.70	0.41	0.073
-40	85.45	0.00	108.00	0.36	0.070
-20	83.27	6.56	104.40	0.32	0.067
0	80.99	13.15	100.70	0.28	0.064
20	78.61	19.81	96.74	0.24	0.061
40	76.08	26.61	92.51	0.21	0.058
60	73.38	33.62	87.84	0.19	0.054
68	71.94	37.24	85.28	0.18	0.053
80	70.43	40.95	82.52	0.16	0.051
100	67.11	48.74	76.26	0.14	0.048
120	63.18	57.20	68.66	0.12	0.045

The temperatures used for liquid density and liquid enthalpy are bubble point temperatures. The rest are mid point temperatures.

**Ideal Gas Properties**

Temp °F	ID. Gas Heat Cap. Btu/lb R	ID. Gas Viscosity cP	ID. Gas Therm Cond Btu/hr.ft.R
-60	0.167	0.0098	0.0048
-40	0.171	0.0103	0.0052
-20	0.175	0.0108	0.0057
0	0.180	0.0113	0.0062
20	0.184	0.0118	0.0066
40	0.189	0.0123	0.0071
60	0.193	0.0128	0.0077
68	0.195	0.0130	0.0079
80	0.198	0.0133	0.0082
100	0.202	0.0138	0.0087
120	0.206	0.0143	0.0093

## Saturated Vapor Properties

Temp °F	Sat Vap Density lb/ft <sup>3</sup>	Sat Vap Viscosity cP	Sat Vap Therm. Cond Btu/hr.ft.R	Speed of Sound ft/s
-60	0.145	0.0092	0.0042	539
-40	0.246	0.0102	0.0050	545
-20	0.404	0.0109	0.0057	550
0	0.633	0.0115	0.0063	553
20	0.954	0.0121	0.0069	553
40	1.39	0.0127	0.0075	550
60	1.98	0.0133	0.0081	544
68	2.35	0.0135	0.0084	539
80	2.77	0.0140	0.0088	534
100	3.83	0.0148	0.0096	519
120	5.28	0.0158	0.0105	501

The temperatures used are dew point temperatures.

## Standard States

Enthalpy (-40 °F, liquid = 0)

Entropy (-40 °F, liquid=0)



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