

## Klea® 407A Physical Property Data Sheet – British Units

Klea® 407A is a blend of HFCs 32, 125 and 134a designed for low-temperature applications in new refrigeration equipment and also for retrofit in many existing systems. For information on the properties and safe handling of Klea® 407A, please refer to the Material Safety Data Sheet supplied with the product or available upon request.

The data presented here represents a combination of measurements and estimation. Mexichem does not guarantee its accuracy and reserves the right to update the information in the future, in the light of the best available knowledge at the time.

### Physical Property Data for Klea® 407A

Property		Units	Value
Bubble Point	(1atm)	°F	-49.9
Dew Point	(1atm)	°F	-38.0
Bubble Point Pressure	(70°F)	psia	163.2
Estimated Critical Temperature		°F	181.4
Latent Heat Vaporization	(Tm=70°F)	Btu/lb	78.92
Trouton's Constant		Btu/lb R	0.251
Coeff. Vol. Therm. Exp.	(liquid, 32-68°F)	°F <sup>-1</sup>	0.00178
Density (sat vapor) at 1atm		lb/ft <sup>3</sup>	0.246

### Equation of State (Martin-Hou)

$$P_r = \frac{X T_r}{V_r - B} + \frac{\sum_{i=1,4}}{i} \frac{(A_i + B_i T_r + C_i \exp(-K T_r))}{(V_r - B)^{(i+1)}}$$

$$T_r = T/T_c, P_r = P/P_c, V_r = V/V_c$$

$$B = 0.0$$

$$X = 3.61723$$

$$K = 5.475$$

$$T_c, P_c, V_c = 640.6 \text{ R}, 658.6 \text{ psia}, 0.032 \text{ cu.ft/lb}$$

$$A_1, B_1, C_1 = -11.33191275, 6.8075753325, -12.83650902$$

$$A_2, B_2, C_2 = 9.1343011237, -5.94976187996, -107.94947217$$

$$A_3, B_3, C_3 = -3.925317714, 0.0, 0.0$$

$$A_4, B_4, C_4 = 0.0, 13.694712938, -1247.8526238$$

Applicable Range: 0-400 psia, 0-180 R superheat

Applicable Range: 0-30 bara, 0-100K superheat

**Saturation Envelope — Bubble Point Temperatures**

$$\text{Bubble Point Temperature } (T_b) = A + BX + CX^2 + DX^3$$

$T_b$  = Bubble Point Temperature in °F

$X = \ln(P)$

P = Pressure in psia

A = - 136.5949

B = 31.7022

C = -1.479621

D = 0.62786

**Saturation Envelope — Dew Point Temperatures**

$$\text{Bubble Point Temperature } (T_d) = A + BX + CX^2 + DX^3$$

$T_d$  = Dew Point Temperature in °F

$X = \ln(P)$

P = Pressure in psia

A = -117.658

B = 26.18071

C = 0

D = 0.475794

**Saturation Envelope — Mid Point Temperatures**

$$\text{Mid Point Temperature } (T_m) = A + BX + CX^2 + DX^3$$

$T_m$  = Average of Dew and Bubble Point Temperatures in °F

$X = \ln(P)$

P = Pressure in psia

A = -126.9154

B = 28.77087

C = -0.696455

D = 0.548338

**Latent Heat Vaporization**

$$Dh_{\text{latent}} = A + BX + CX^2 + DX^3 + EX^4$$

Where  $x = (1 - (T_m/T_c))^{(1/3)}$

A = -49.2509

B = 343.1947

C = -281.565

D = 140.195

E = 0 A = -114.4811

$T_m$  = Mid Point Temperature R

$T_c$  = Critical Temperature R

$T_c = 640.6$  R

$dh_{\text{latent}} = \text{Btu/lb}$

### Ideal Gas Heat Capacity

$$C_p \text{ (ideal)} = A + BT + CT^2 + D/T$$

A = 0	T = Temperature R
B = 0.00038745	Cp(ideal) = Btu/lb R
C = -1.191E-07	
D = 12.058506	

### Saturated Liquid Enthalpy

$$H_{\text{liquid}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{where } x = (1 - (T_b/T_c))^{(1/3)}$$

A = 131.38117	T <sub>b</sub> = Bubble Point Temperature R
B = -202.8418	T <sub>c</sub> = Critical Temperature R
C = 201.7119	T <sub>c</sub> = 640.6 R
D = -256.1254	h <sub>liquid</sub> = Btu/lb
E = 0	

### Liquid Density

$$P_{\text{liquid}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{where } x = (1 - (T_b/T_c))^{(1/3)}$$

A = -22.2403	T <sub>b</sub> = Bubble Point Temperature R
B = 324.5572	T <sub>c</sub> = Critical Temperature R
C = -416.6396	T <sub>c</sub> = 640.6 R
D = 249.6117	P <sub>liquid</sub> = lb/ft <sup>3</sup>
E = 0	

### Liquid Viscosity

$$\ln (\mu)_{\text{liquid}} = A + B/T_m + CT_m$$

A = 3.148664	μ <sub>liquid</sub> = Cp
B = -327.43764	T <sub>m</sub> = Mid Point Temperature R
C = -0.0081733	

### Liquid Thermal Conductivity

$$K_{\text{liquid}} = A + BX + CX^2 + DX^3$$

$$\text{where } x = (1 - (T_m/T_c))^{(1/3)}$$

A = 0.0352464	T <sub>c</sub> = 640.6 R
B = -0.0177842	K <sub>(liquid)</sub> = Btu/hr.ft.R
C = 0.0391964	T <sub>m</sub> = Mid Point Temperature R
D = 0.0722151	T <sub>c</sub> = Critical Temperature R

**Saturated Vapor Density**

$$P_{\text{vapor}} = A + BX + CX^2 + DX^3 + EX^4$$

$$\text{Where } x = (1 - (T_d/T_c))^{(1/3)}$$

A = 33.90555	T <sub>d</sub> = Dew Point Temperature R
B = -76.47105	T <sub>c</sub> = Critical Temperature R
C = 21.41245	T <sub>c</sub> = 640.6 R
D = 27.51538	P <sub>vapor</sub> = lb/ft <sup>3</sup>
E = 0	

**Vapor Viscosity (Ideal Vapor)**

$$\mu_{\text{vapor}} = A + BT + CT^2$$

A = -0.001349	$\mu_{\text{vapor}} = \text{Cp}$
B = 0.00002988	
C = -4.676E-09	
T = Temperature	

**Vapor Viscosity (Sat Vapor)**

$$\mu_{\text{vapor}} = A + BT_d + CT_d^2 + D/T_d^3$$

A = -0.079123	$\mu_{\text{vapor}} = \text{Cp}$
B = 0.00053269	T <sub>d</sub> = Dew Point Temperature R
C = -1.09023E-06	
D = 7.84820E-10	

**Vapor Thermal Conductivity (Ideal Vapor)**

$$K_{\text{vapor}} = A + BT + CT^2$$

A = -0.0025242	T = Temperature R
B = 0.00001397	K(vapor) = Btu/hr.ft.R
C = 1.12407E-08	

**Vapor Thermal Conductivity (Sat Vapor)**

$$K_{\text{vapor}} = A + BT_d + CT_d^2 + D/T_d^3$$

A = -0.0559971	K(vapor) = Btu/hr.ft.R
B = 0.00035354	T <sub>d</sub> = Dew Point Temperature R
C = -7.11567E-07	
D = 5.17638E-10	

**Speed of Sound (Sat Vapor)**

$$\mu_{\text{vapor}} = A + BT_d + CT_d^2 + D/T_d$$

A = -2993.2087  
 B = 9.38958151  
 C = -0.0079965  
 D = 416651.575

$\mu_{\text{(vapor)}} = \text{ft/s}$   
 $T_d = \text{Dew Point Temperature R}$

**Saturation Envelope**

Pressure psia	Temperatures °F		
	BUB pnt	MID pnt	DEW pnt
10.0	-63.8	-57.7	-51.6
14.7	-49.9	-44.0	-38.0
20.0	-38.0	-32.2	-26.4
30.0	-21.2	-15.5	-9.9
50.0	2.4	7.8	13.2
70.0	19.5	24.8	30.1
100.0	39.3	44.4	49.4
150.0	64.1	68.7	73.4
200.0	83.2	87.5	91.8
250.0	99.0	103.0	107.0
300.0	112.6	116.3	120.0
350.0	124.6	127.9	131.3
400.0	135.3	138.4	141.5

**Liquid Properties**

Temp °F	Liquid Density lb/ft <sup>3</sup>	Liquid Enthalpy Btu/lb	Latent Heat Btu/lb	Liquid Viscosity cP	Liq Therm Cond Btu/hr.ft.R
-60	88.83	-6.27	104.5	0.39	0.07
-40	86.55	0	101.3	0.35	0.067
-20	84.23	6.34	97.9	0.3	0.064
0	81.85	12.79	94.3	0.27	0.061
20	79.38	19.36	90.4	0.23	0.058
40	76.77	26.09	86.2	0.2	0.055
60	73.96	33.05	81.4	0.18	0.052
68	72.76	35.91	79.4	0.17	0.05
80	70.84	40.31	76.1	0.15	0.048
100	67.25	48.03	69.8	0.13	0.045
120	62.84	56.46	62.1	0.12	0.042

The temperatures used for liquid density and liquid enthalpy are bubble point temperatures. The rest are mid point temperatures.

## Ideal Gas Properties

Temp °F	ID. Gas Heat Cap. Btu/lb R	ID. Gas Viscosity cP	ID. Gas Therm Cond Btu/hr.ft.R
-60.00	0.166	0.0098	0.0049
-40.00	0.170	0.0104	0.0053
-20.00	0.175	0.0109	0.0058
0.00	0.179	0.0114	0.0063
20.00	0.184	0.0119	0.0068
40.00	0.188	0.0124	0.0073
60.00	0.192	0.0129	0.0078
68.00	0.194	0.0131	0.0080
80.00	0.197	0.0134	0.0083
100.00	0.201	0.0139	0.0088
120.00	0.205	0.0144	0.0094

## Saturated Vapor Properties

Temp °F	Sat Vap Density Lb/ft <sup>3</sup>	Sat Vap Viscosity cP	Sat Vap Therm. Cond Btu/hr.ft.R	Speed of Sound ft/s
-60.00	0.212	0.0097	0.0047	524.7
-40.00	0.298	0.0104	0.0053	531.8
-20.00	0.463	0.0110	0.0059	536.9
0.00	0.721	0.0116	0.0064	539.7
20.00	1.091	0.0122	0.0070	539.4
40.00	1.598	0.0128	0.0076	535.8
60.00	2.278	0.0134	0.0082	528.5
68.00	2.610	0.0137	0.0085	524.5
80.00	3.185	0.0142	0.0089	517.2
100.00	4.402	0.0151	0.0097	501.6
120.00	6.077	0.0162	0.0107	481.4

The Temperatures used are dew point temperatures.

Standard States

Enthalpy (-40°F, liquid = 0)

Entropy (-40°F, liquid = 0)

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